

Recent Improvements for the Ammonia Fiber Explosion (AFEX) Process and Resulting Reductions in Projected Ethanol Prices

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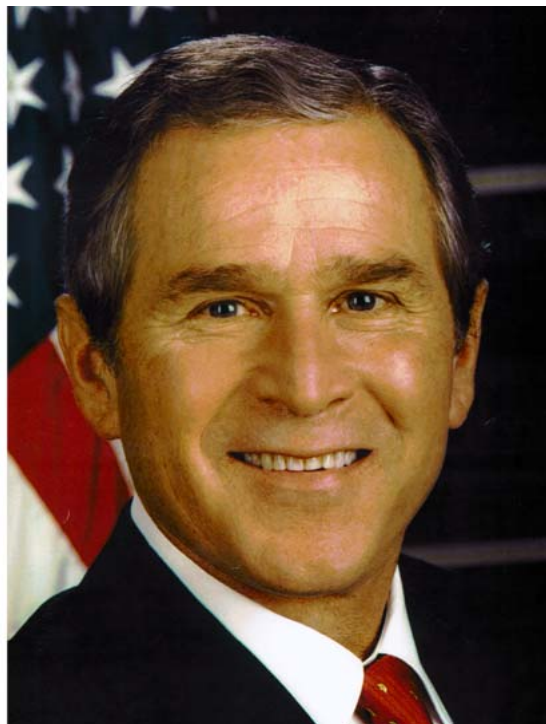
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Thank You Mr. President



Ethanol Production from Enzymatic Hydrolysates of AFEX-Treated Coastal Bermudagrass and Switchgrass

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“... We'll also fund additional research in cutting-edge methods of **producing ethanol...from** wood chips and stalks, or **switch grass...**”

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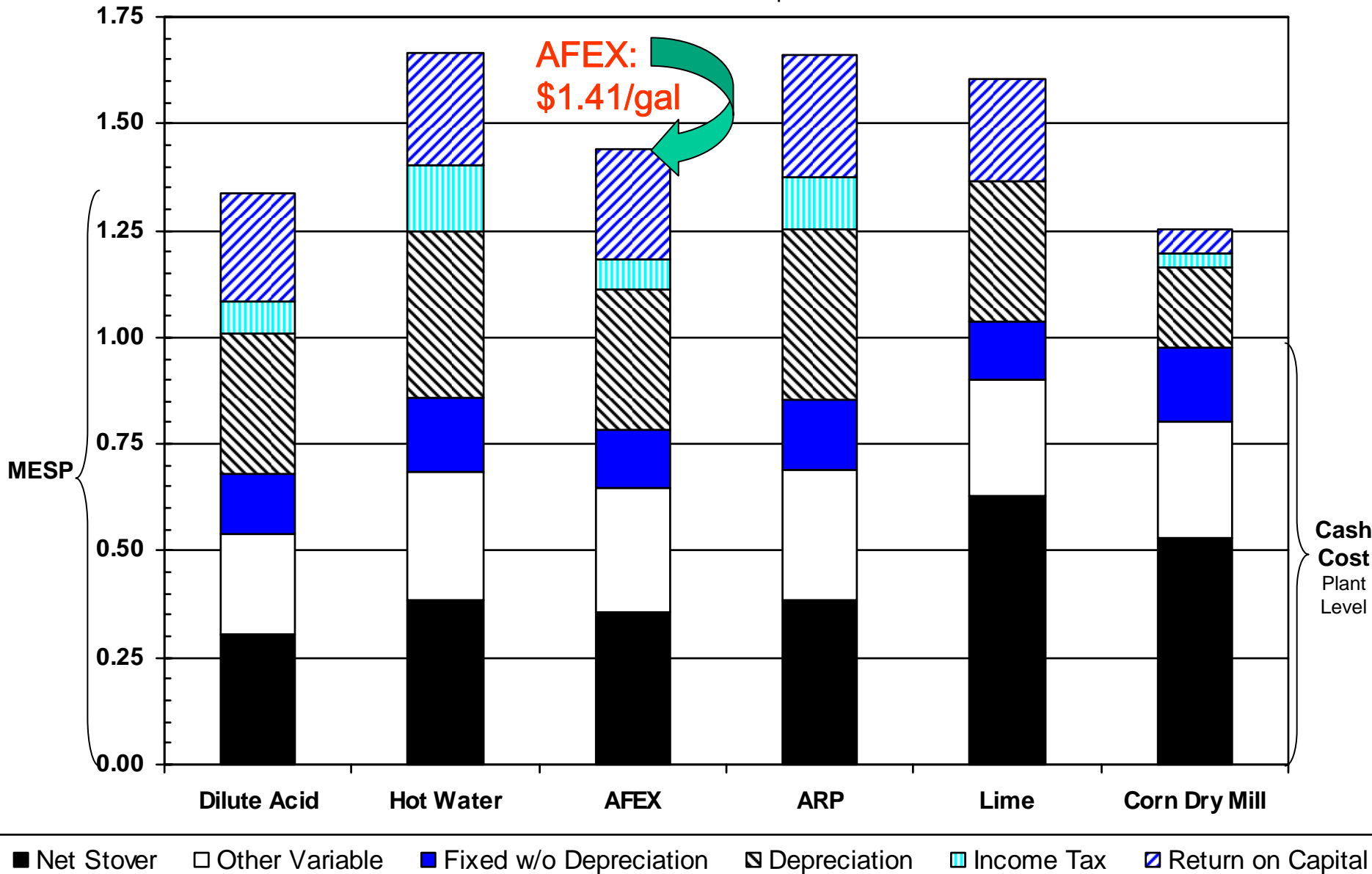
How We Got Here

- Two years ago, CAFI team did techno-economic comparisons of leading pretreatments*
- Ammonia Fiber Explosion (AFEX) Minimum Ethanol Selling Price (MESP) ~ \$1.40/gallon
- Key AFEX process economic parameters identified
- MSU & collaborators at Dartmouth worked on AFEX improvements during last two years
- We report here our results:
 - Improved AFEX process parameters
 - Improved ammonia recovery approach
 - These two improvements reduce MESP by ~\$0.40/gallon and are “ready to build”
 - Integration of AFEX with consolidated bioprocessing (CBP) in “mature biorefinery” scenario reduces costs another ~\$0.20/gal
 - CBP option is **not** “ready to build”
- * *Our sincere thanks to NREL & Dr. Tim Eggeman*

Pretreatment Economic Analysis: CAFI Team

\$/gal EtOH

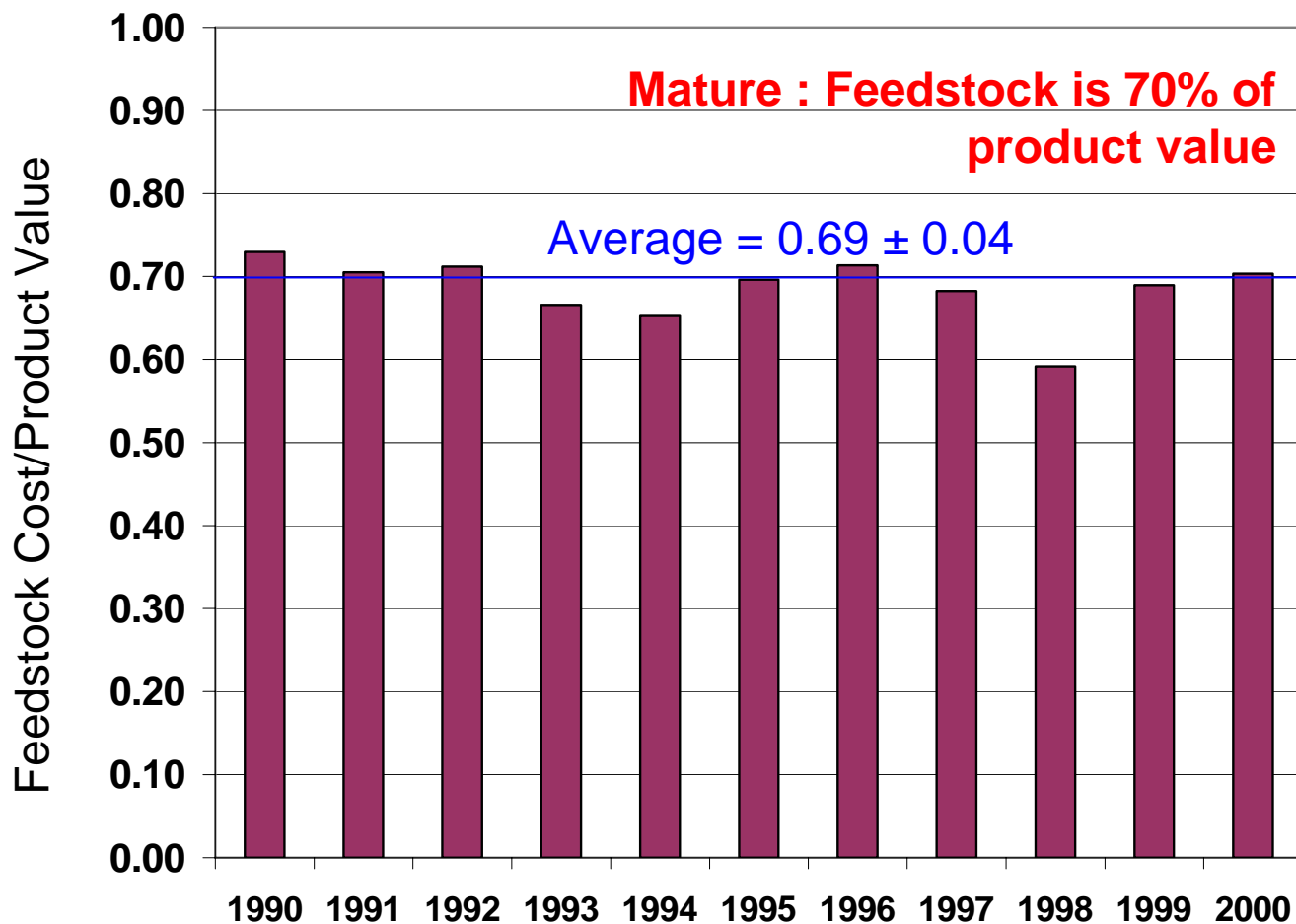
Proof Year: 4th Year of Operation



Key Findings: AFEX Economic Analysis

- Reduce ammonia loadings (kg NH₃/kg dry biomass)
- Reduce required ammonia recycle concentrations (manage system water)
- Reduce capital cost of AFEX
- Reduce enzyme loadings for >90% conversion of glucan plus xylan
- AFEX is not a “mature” process
- Neither is overall cellulosic ethanol process

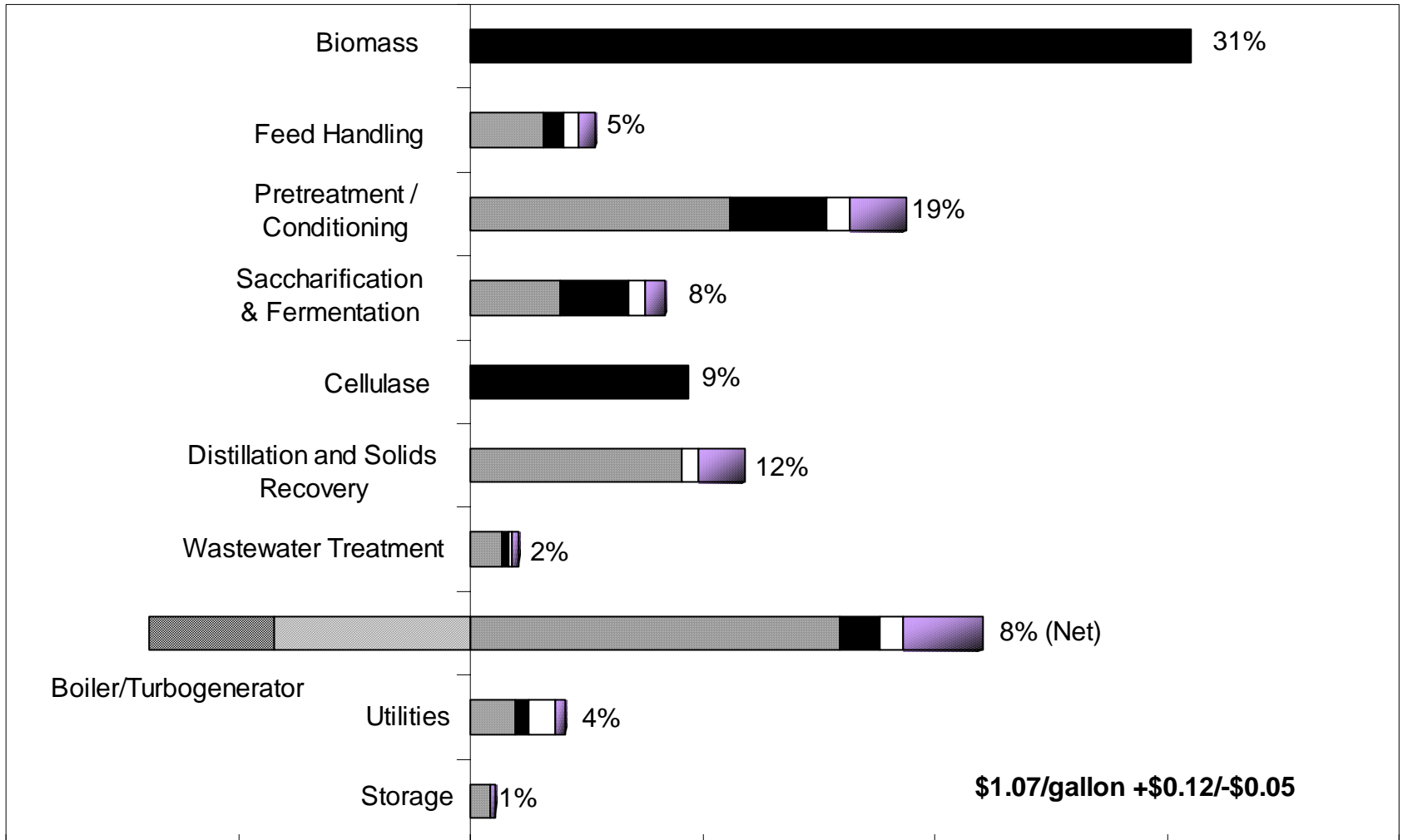
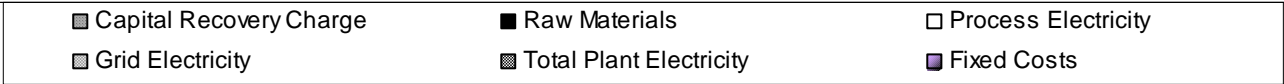
U.S. Petroleum Refining Feedstock Cost/Product Value, 1990-2000



Sources: Yields: API, Basic Petroleum Databook; Prices: EIA, Petroleum Marketing Annual; *Oil & Gas Journal* database.

NREL Design Report (\$2002)

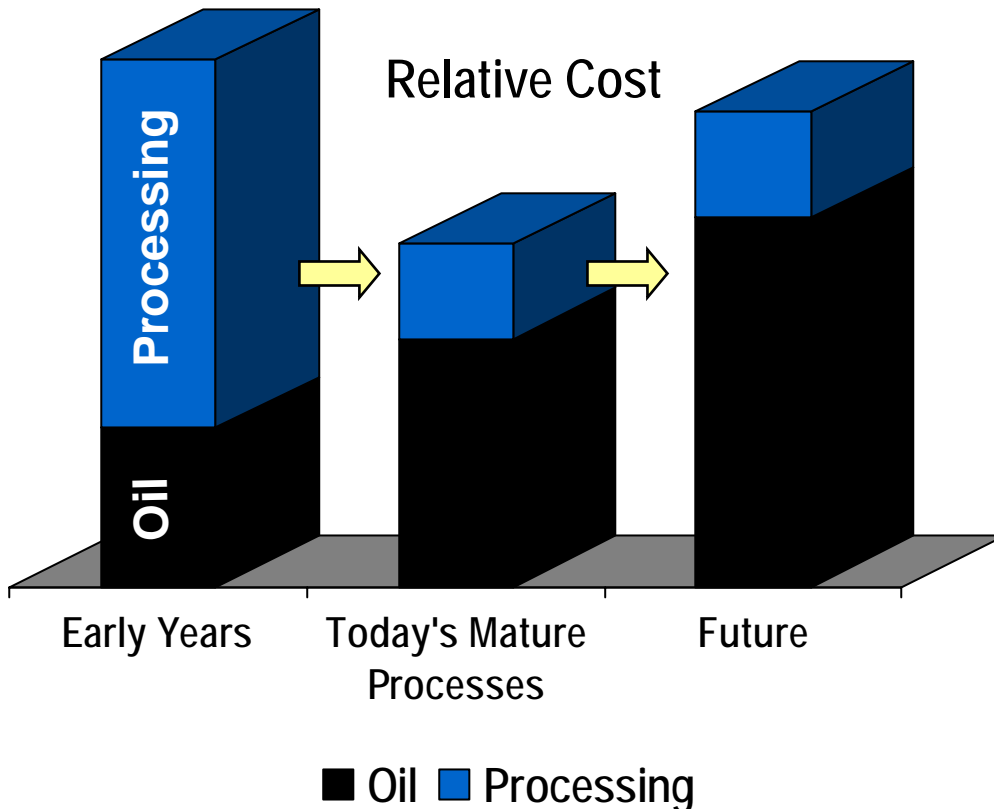
(June 2002 NREL/TP-510-32438 by Aden, *et al*)



\$1.07/gallon + \$0.12/- \$0.05

-20% -10% 0% 10% 20% 30% 40%

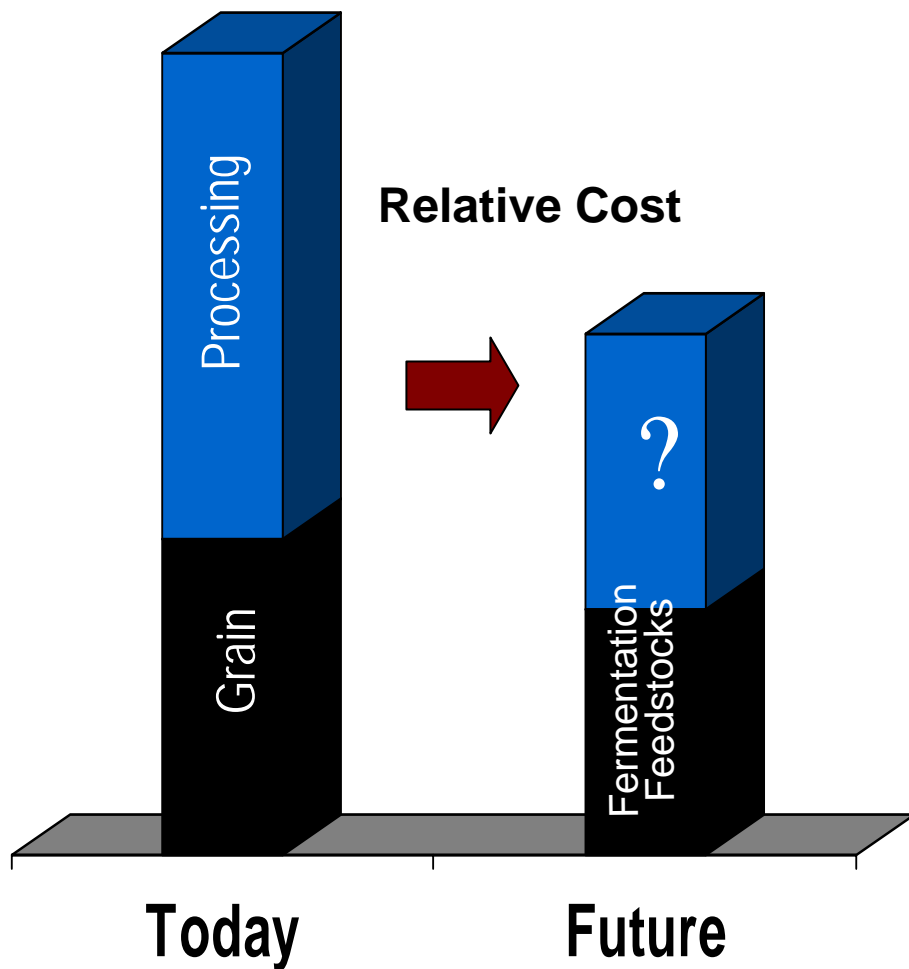
Impact of Processing Improvements: Oil's Past & Future



- Historically, petrochemical processing costs exceeded feedstock costs
- Petroleum processing efficiencies have increased and costs have decreased dramatically but reaching point of diminishing returns
- Petroleum raw materials have long-term problems which will NOT improve
 - Costs will continue to increase as supplies tighten
 - High price variability
 - Impacts national security
 - Climate security concerns
 - Not renewable
- **Not a pretty future for oil--or for our oil dependent society**

Adapted from J. Stoppert, 2005

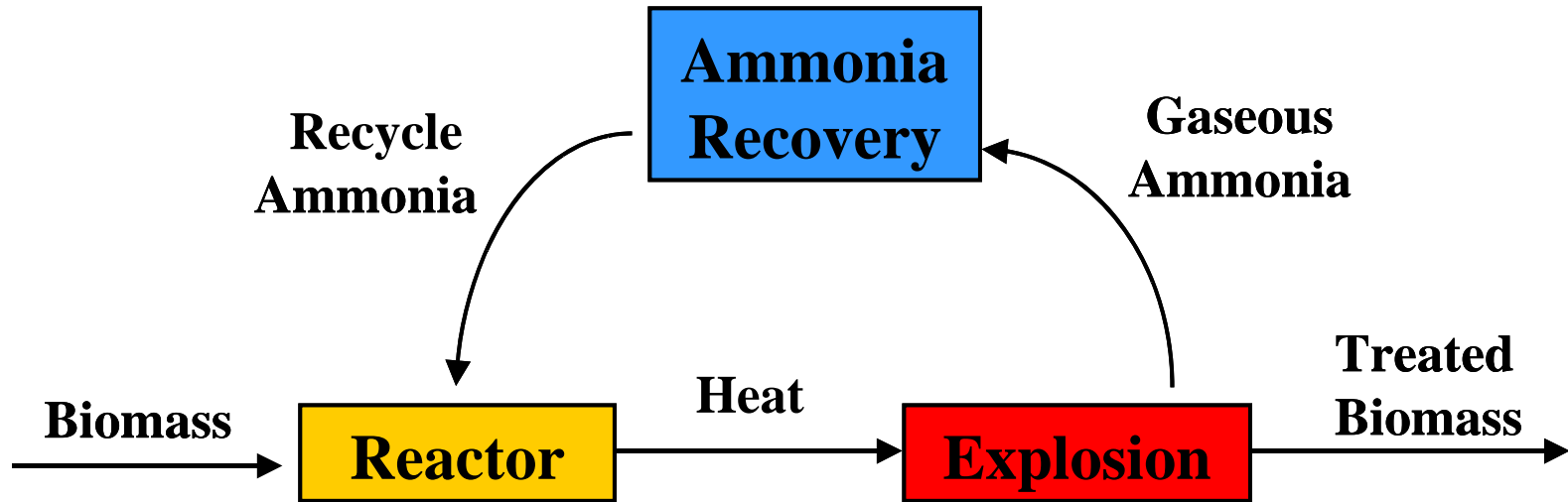
Impact of Processing Improvements: The Future of Biomass Conversion



- Processing costs dominate cellulosic ethanol today
- Cellulosic raw material costs should be stable or decrease
 - Renewable resource
 - Potential for very large yield increases
- Biomass processing costs **will** decrease: Key question is *how far* and *how fast*
- For ethanol from cellulose:
 - Pretreatment costs
 - Enzyme costs
 - Fermentation costs
- **Pretreatment affects all other downstream operations**

Adapted from J. Stoppert, 2005

How does AFEX pretreatment work?



- Biomass heated (~100 C) with concentrated ammonia
- Rapid pressure release ends treatment
- 99% of ammonia is recovered & reused, remainder serves as N source downstream for fermentation
- No sugar degradation, relatively mild conditions
- No hydrolysis to sugar monomers, xylooligomers formed

Evolution of Biomass Processing Featuring Enzymatic Hydrolysis

Biologically-Mediated Event

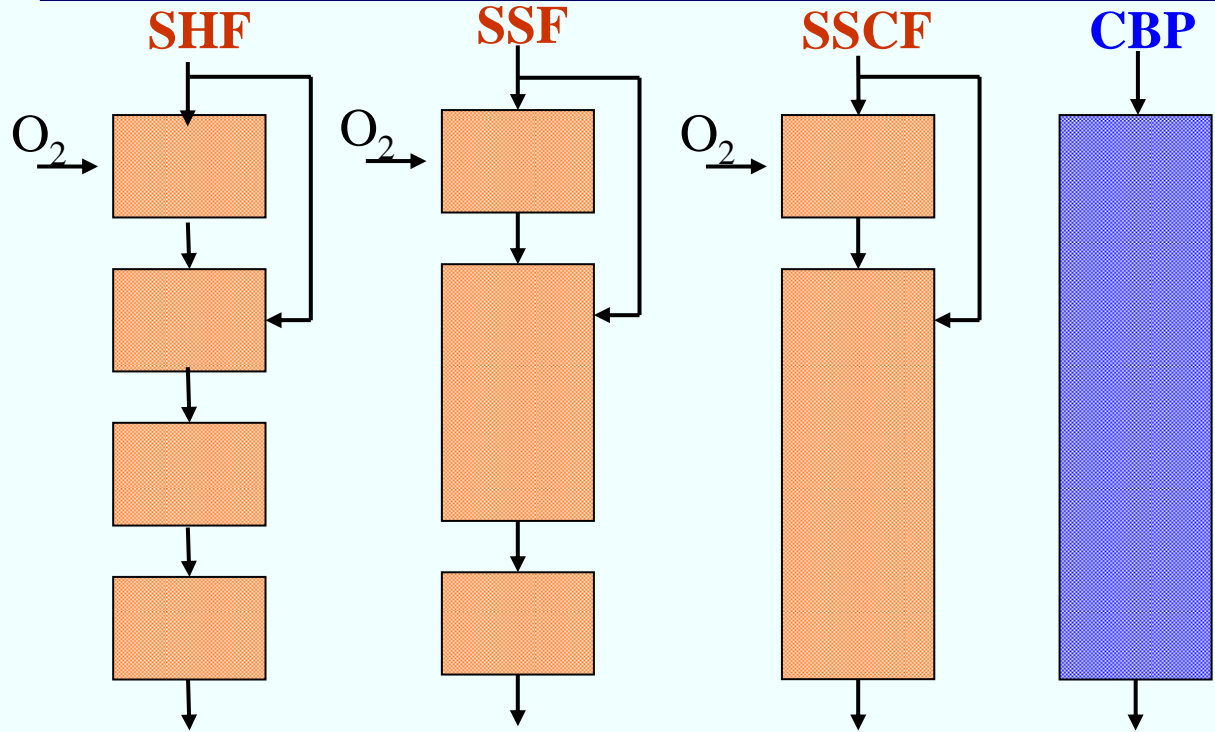
Processing Strategy
(each box represents a bioreactor - not to scale)

Cellulase production

Cellulose hydrolysis

Hexose fermentation

Pentose fermentation



SHF: Separate hydrolysis & fermentation

SSF: Simultaneous saccharification & fermentation

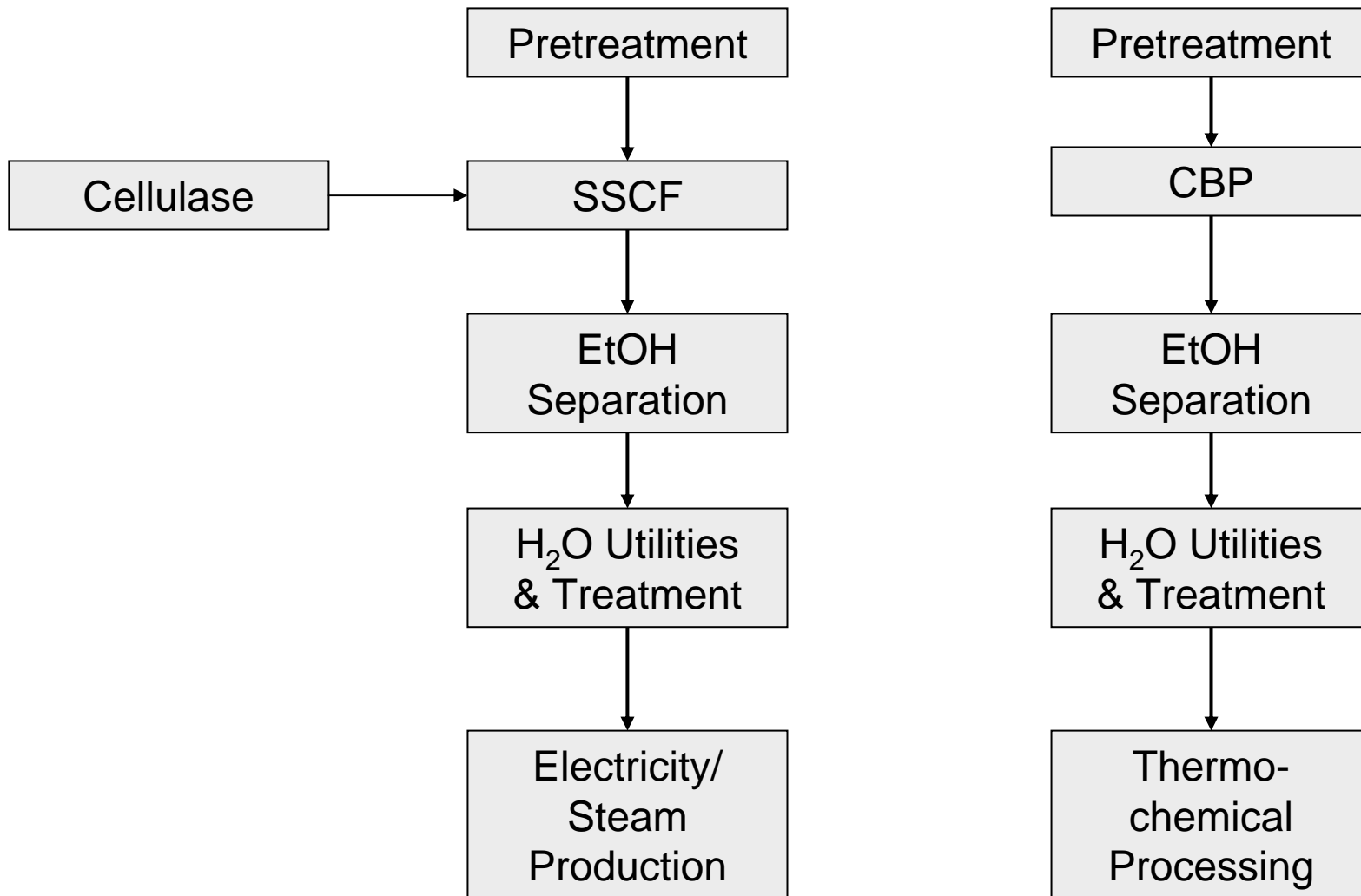
SSCF: Simultaneous saccharification & co-fermentation

CBP: Consolidated bioprocessing

Process Modeling Context

- NREL Approach (nearer term)
 - NREL/Eggeman
 - SSCF
 - 2,000 dry ton/day
 - Feedstock washing
 - AFEX pretreatment; old process parameter
 - Ammonia recompression recovery
 - Evaporation of still bottoms
- “Mature technology” RBAEF Approach
 - Dartmouth/RBAEF team
 - 5,000 dry ton/day
 - No feedstock washing
 - AFEX pretreatment
 - New ammonia recovery approach
 - Heat pumps
 - Evaporation of still bottoms eliminated
 - Other changes

Overall Process

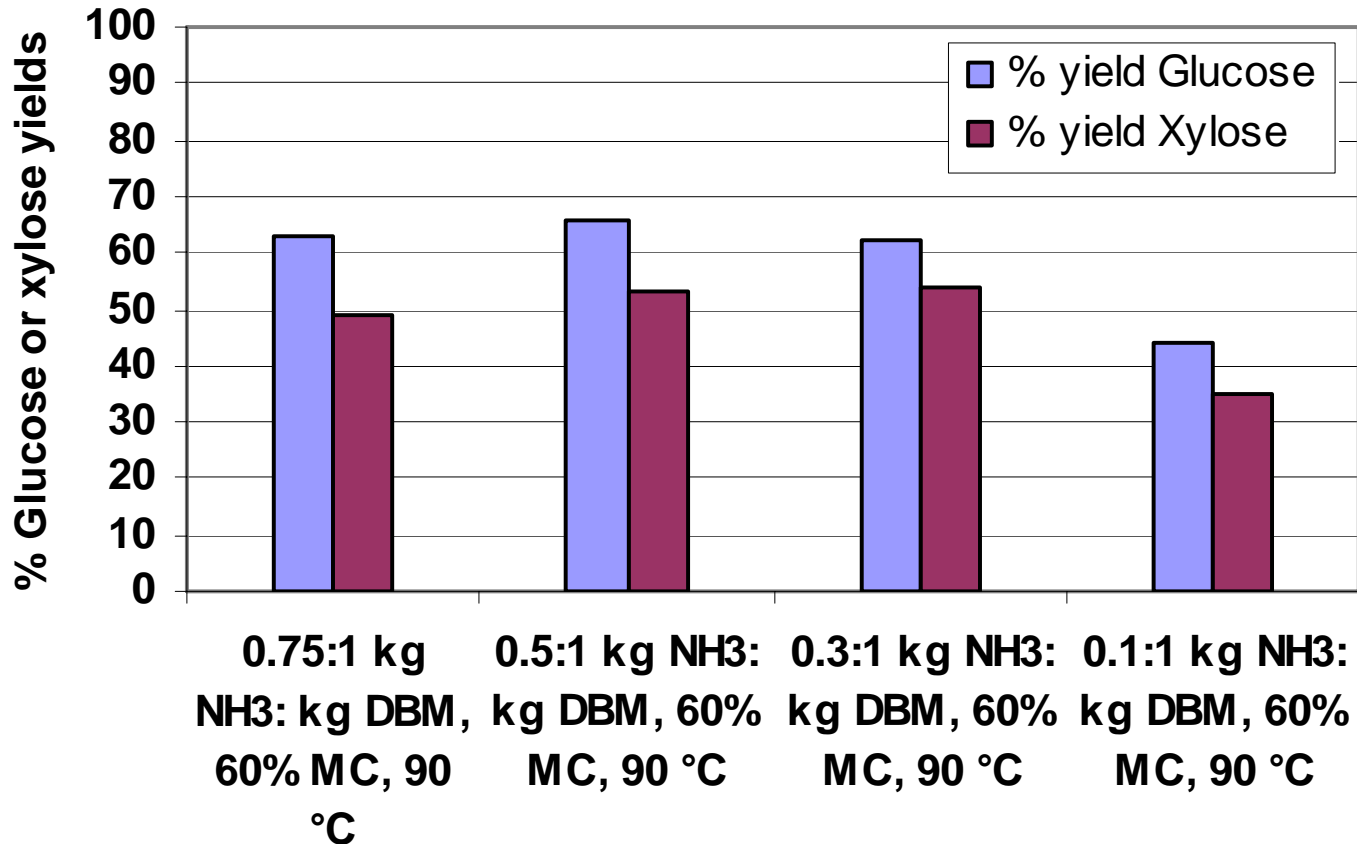


Process Improvements

- Report technoeconomic advances in
 - AFEX process parameters: reduce ammonia loading & ammonia recycle concentration
 - AFEX process design: trade recompression for quench system
 - AFEX integration with advanced bioconversion by CBP
- Some details of new lower capital cost ammonia recovery approach
- Cumulative effect of all changes cuts \$0.60/gallon from MESP
- Have not yet estimated economic effects of enzyme synergies (reduce total enzyme loadings?) between cellulase and xylanase

Reducing Ammonia Loading

Key is to keep ammonia in liquid phase:
minimize ammonia vaporization



16 hr yields
15 FPU cellulase/gm glucan

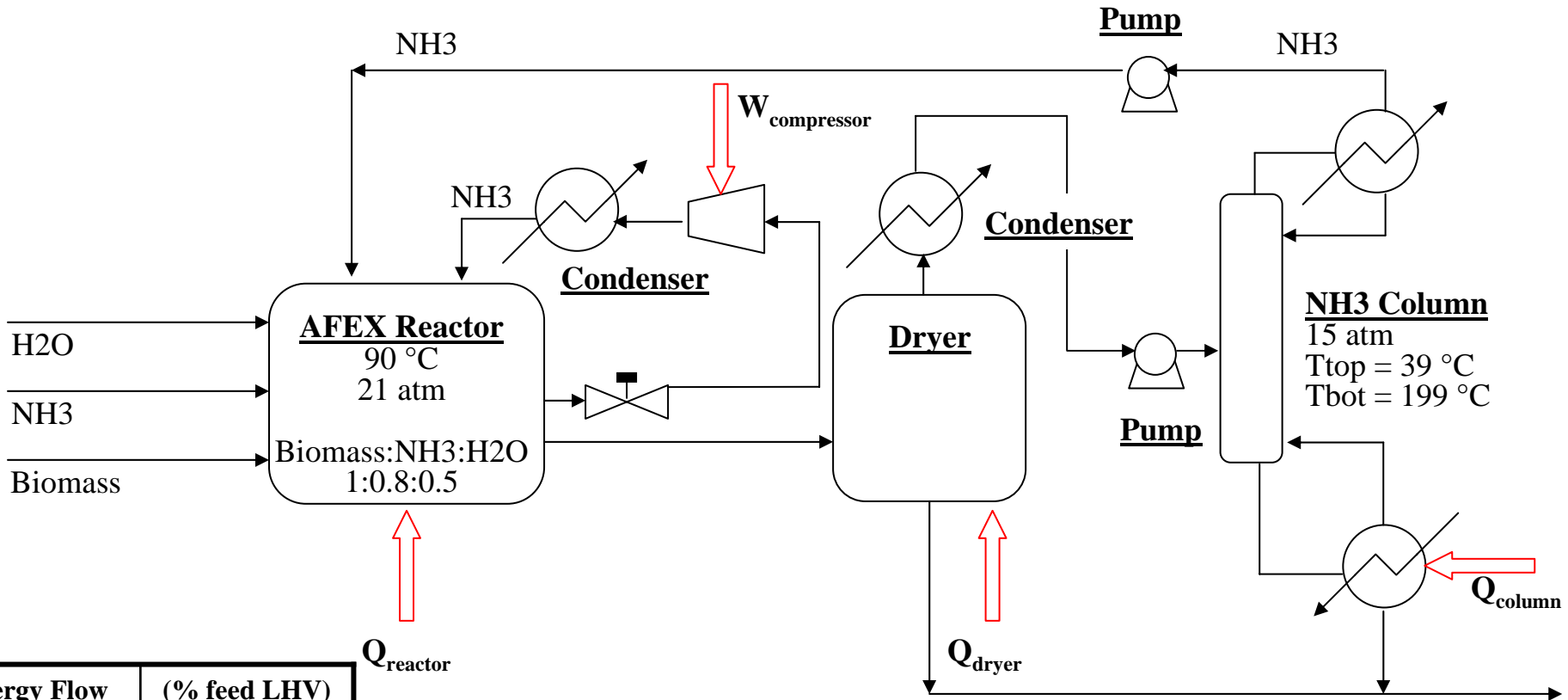
AFEX treatment conditions

Managing Ammonia & Water in AFEX for High Sugar Yields*

Ammonia Distribution	Water Distribution	% Sugar Yields G/X
All as NH ₃	All in stover	93.0/74.3
$\frac{3}{4}$ NH ₃ ; $\frac{1}{4}$ NH ₄ OH	$\frac{1}{2}$ NH ₄ OH; $\frac{1}{2}$ stover	93.0/78.9
“” “”	All in NH ₄ OH	79.9/64.9
$\frac{1}{2}$ NH ₃ ; $\frac{1}{2}$ NH ₄ OH	All in NH ₄ OH	57.7/47.9
“” “”	$\frac{1}{2}$ NH ₄ OH; $\frac{1}{2}$ stover	97.8/82.0
All NH ₄ OH	All NH ₄ OH	71.0/57.0
“” “”	$\frac{3}{4}$ NH ₄ OH; $\frac{1}{4}$ stover	97.1/79.0

Uniform final conditions: 1:1 NH₃:stover; 60% moisture DWB; 90 C

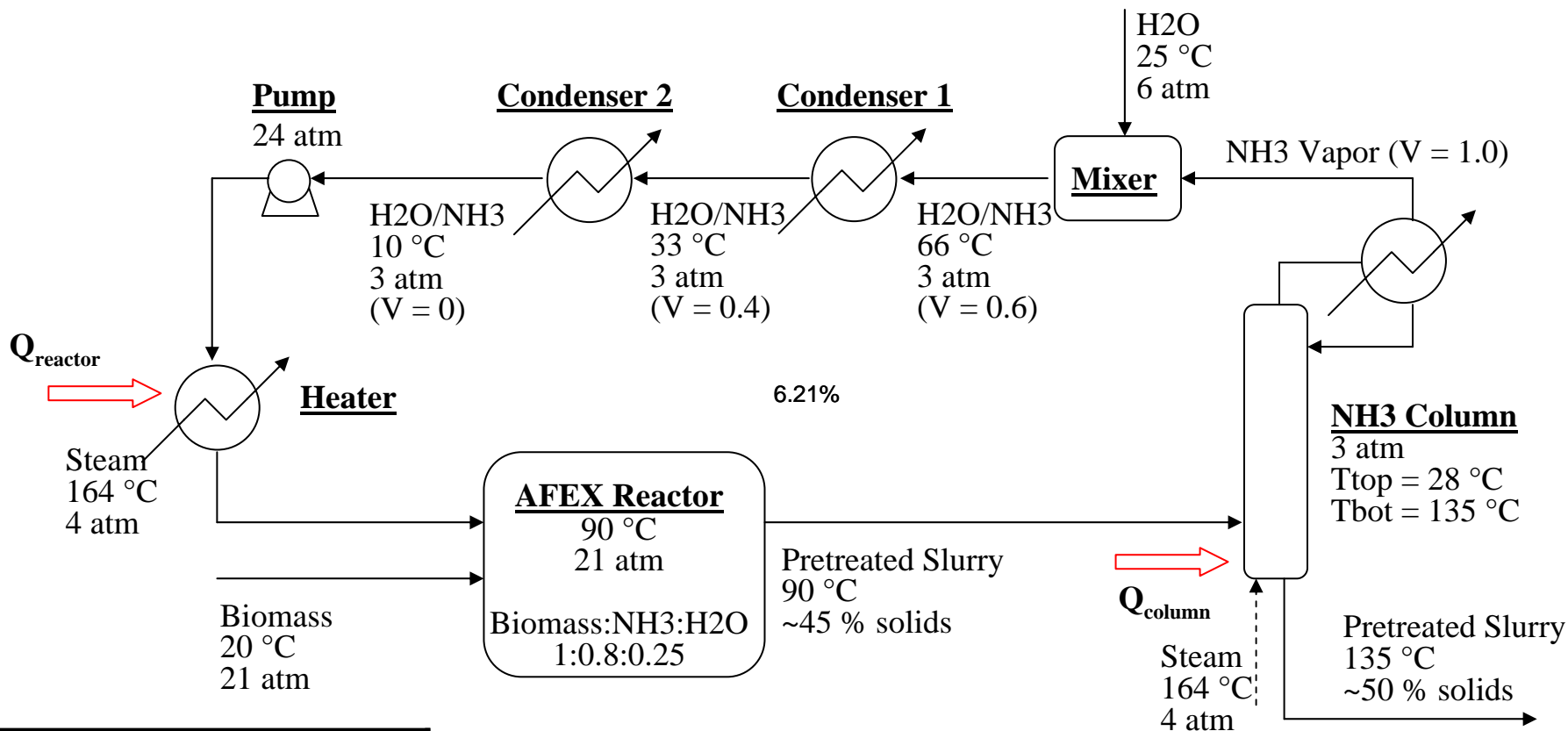
AFEX Pretreatment (Recompression) Flash + Distillation NH₃ Recovery



Energy Flow	(% feed LHV)
$Q_{reactor}$	0%
Q_{dryer}	8.4%
Q_{column}	3.7%
$W_{compressor}$	0.5%
TOTAL	12.6%

AFEX Pretreatment (New Approach)

Distillation w/Quench Condensation NH₃ Recovery

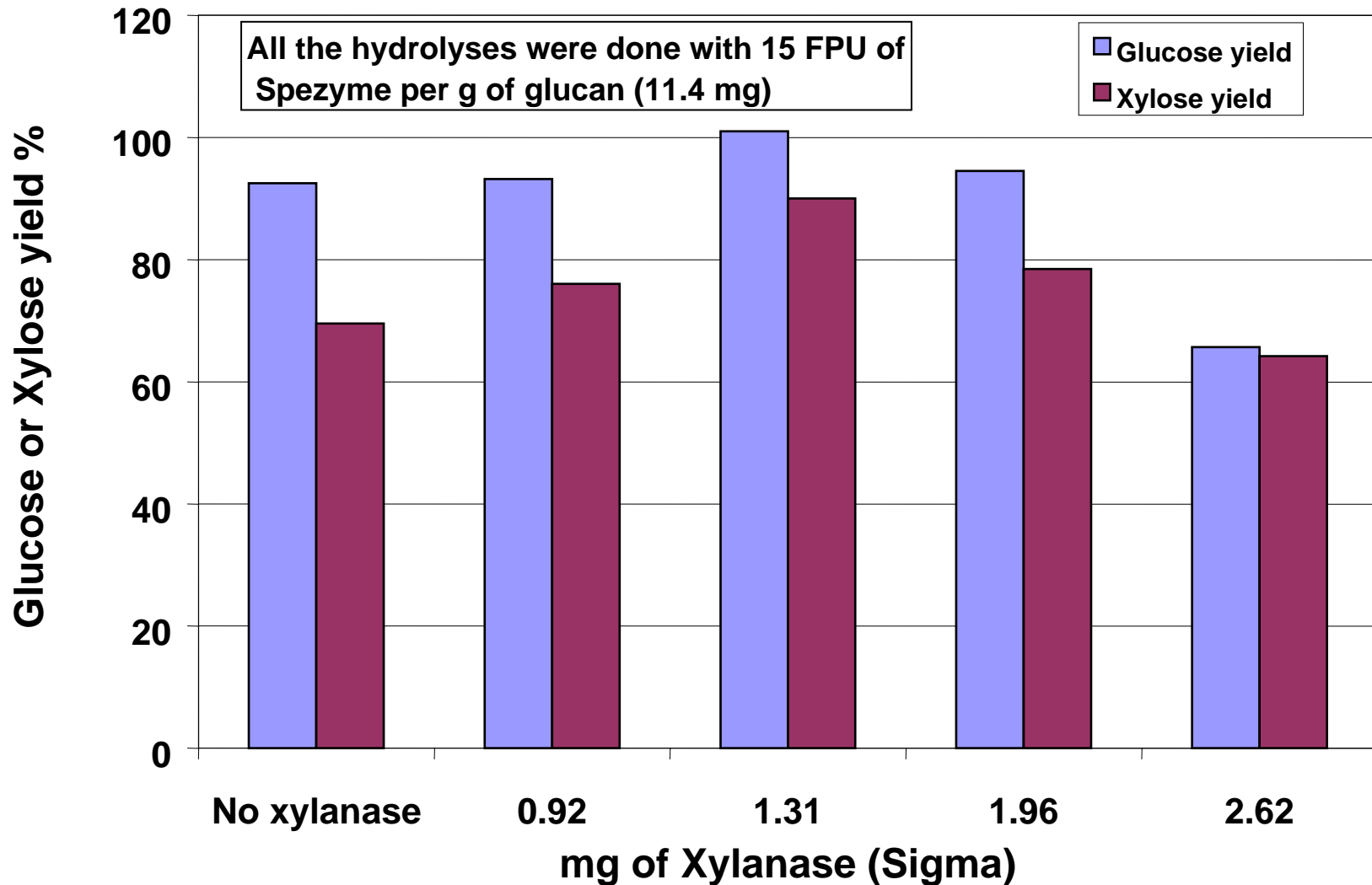


Energy Flow	(% feed LHV)
Q_{reactor}	0%
Q_{column}	6.21%
$W_{\text{chilled water}}$	0.75%
TOTAL	6.95%

Note: 3 atm (upper limit to keep T column < 140 °C at bottom)

Effects of adding xylanase: AFEX treated corn stover

Glucose and xylose yields after 168 hr of hydrolysis



AFEX Pretreatment & CBP

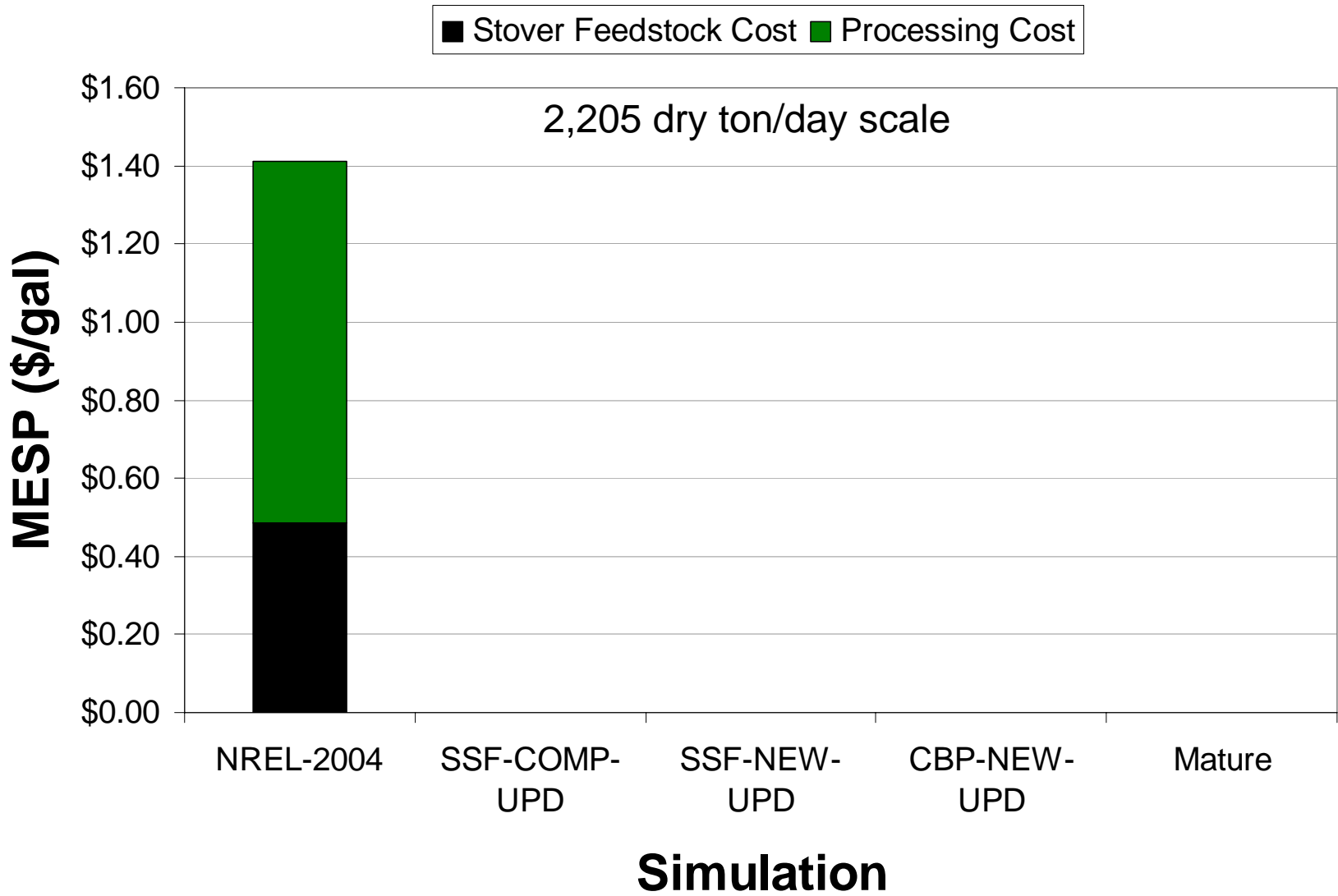
- Have shown nearer term (“buildable today”) results with AFEX and SSCF
- Have not yet exploited “enzyme cost lever”
 - Tailor enzyme mixture for AFEX treated biomass
 - Exploit cellulase/xylanase synergies for AFEX
- Longer term RBAEF approach “mature” technology would use
 - AFEX
 - CBP
 - Many other advances
- What do economics look like with these current and future advances?

Effects of AFEX Process Improvements: New Cost Estimates (w/out Reduced Enzyme)*

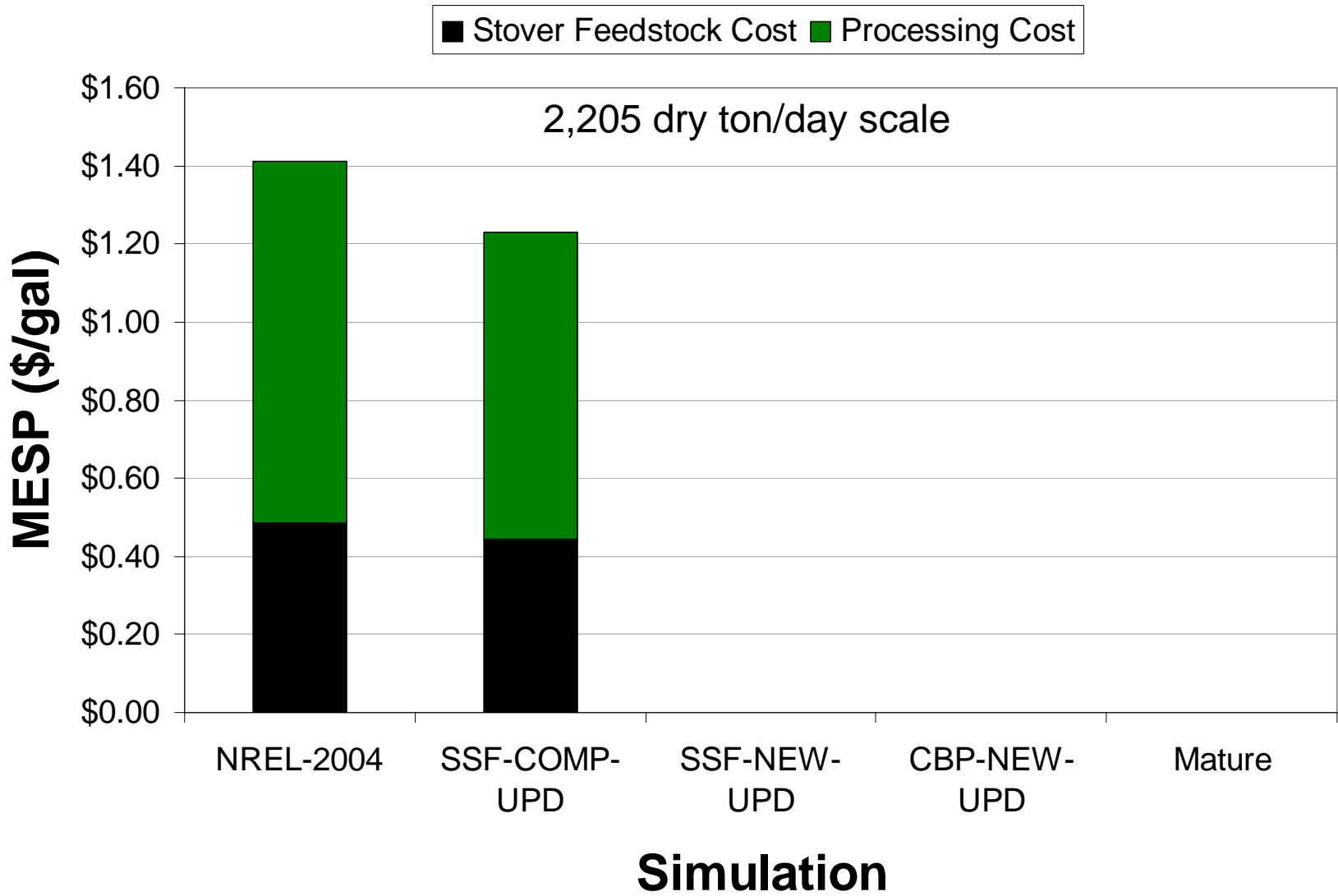
Abbreviation	Meaning
NREL-2004	SSCF, NH ₃ Recompression, Old AFEX parameters
SSF-COMP-UPD	SSCF, NH ₃ Recompression, Updated AFEX parameters
SSF-NEW-UPD	SSCF, New NH ₃ Recovery approach, Updated AFEX parameters
CBP-NEW-UPD	CBP, New NH ₃ Recovery approach, Updated AFEX parameters
Fully Mature	Cost 70% Feedstock, 30% Processing

*Assumes 2,200 tons per day scale

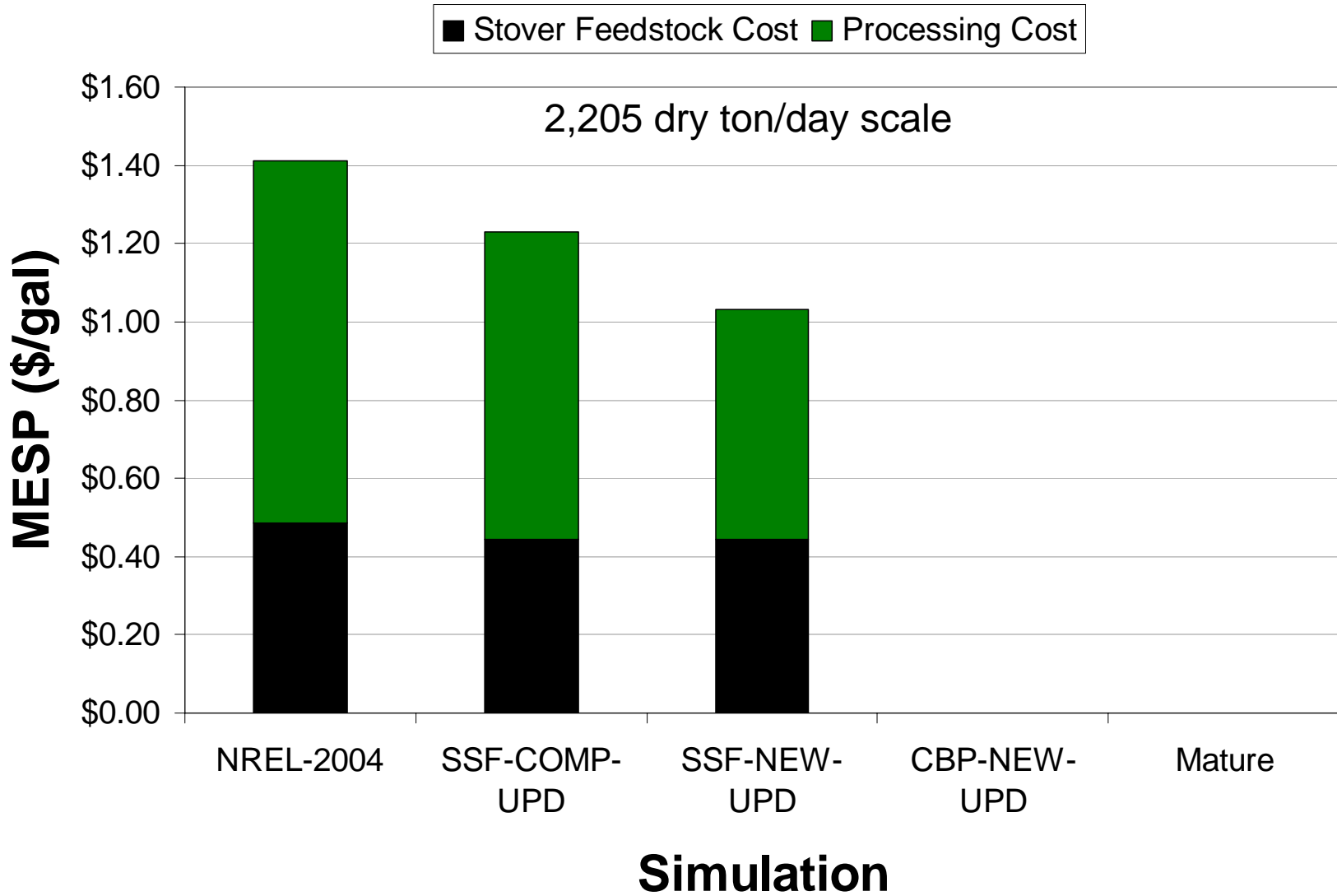
Final Results



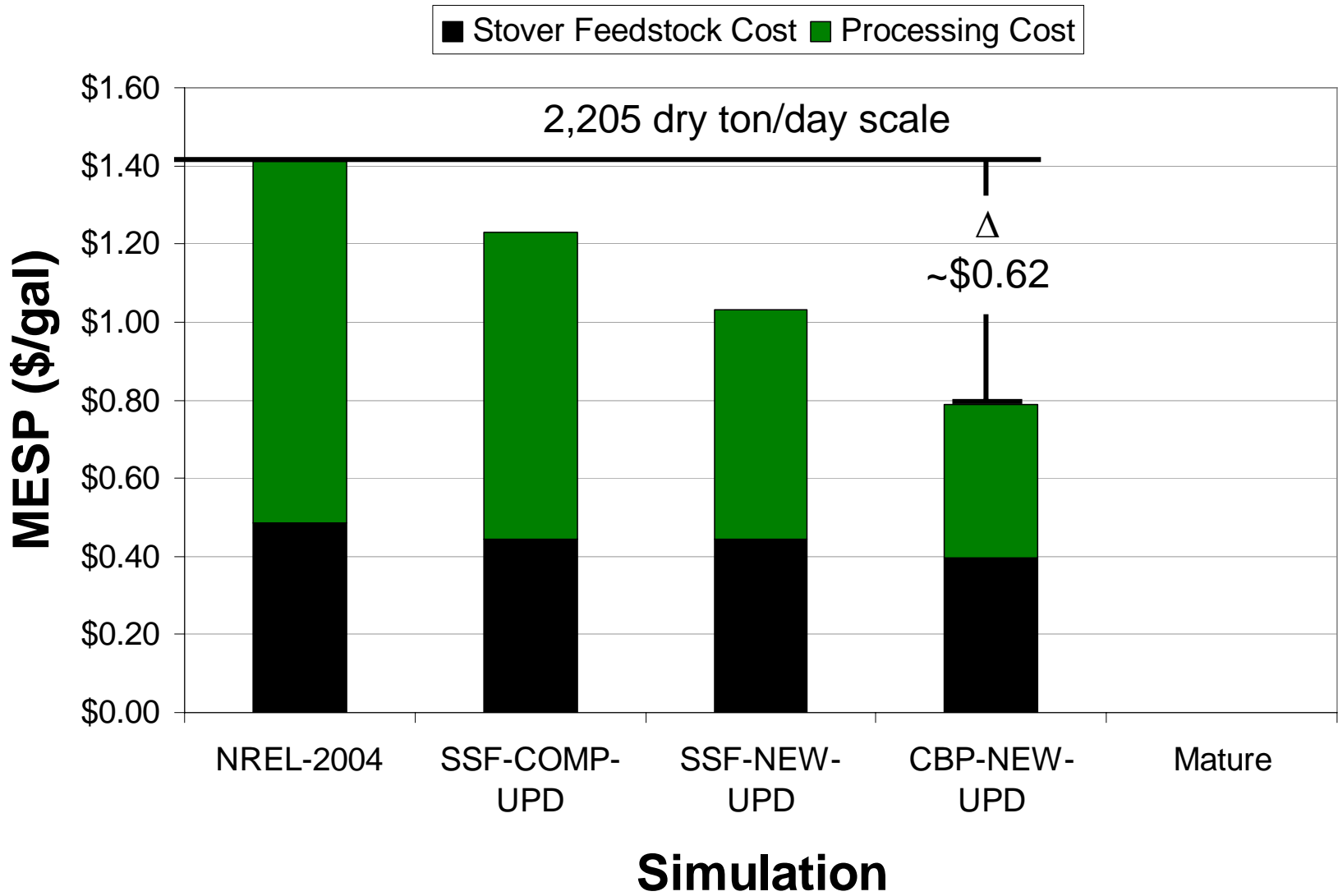
Final Results



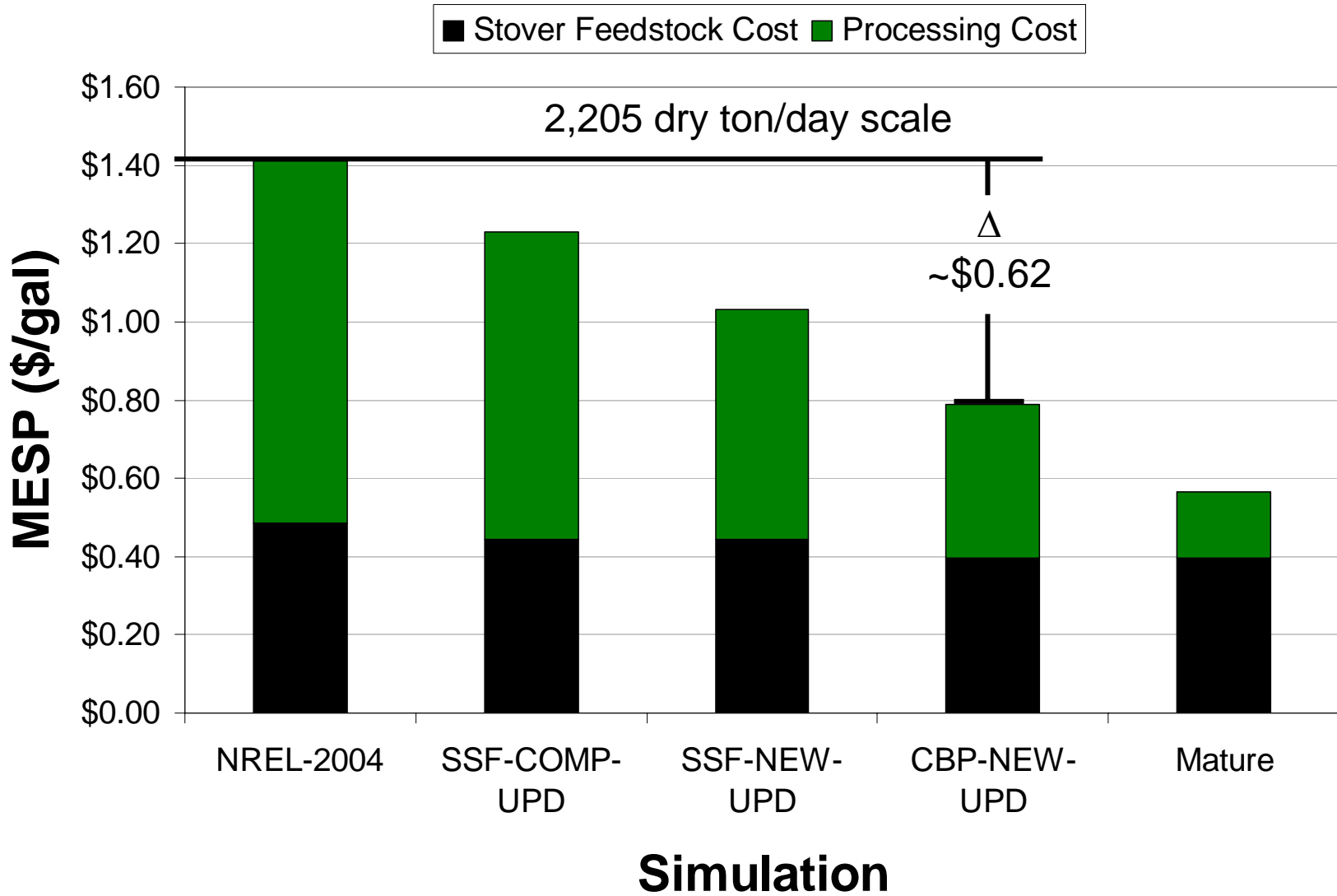
Final Results



Final Results



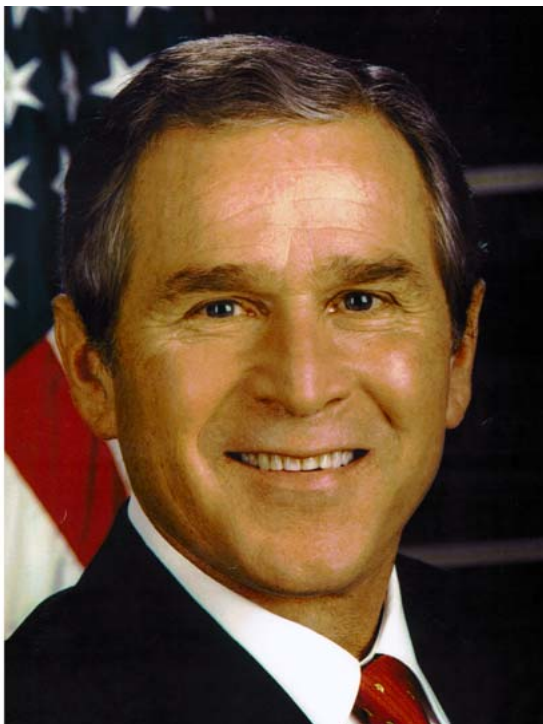
Final Results



In Summary

- Large scale cellulosic ethanol is nearer than many think
 - Processes improving rapidly: pretreatment, enzymes, fermentations
 - Favorable raw material costs
- Increased awareness of oil “externalities”
- Venture capital & (we hope) increased R&D funding
- \$60 per barrel (and up) oil
- High level political support

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Questions?



- Thank You for Your Attention
- Thanks to All Our Collaborators
- For Further Information Visit www.everythingbiomass.org

Relative Cost Contribution by Area: Processing Dominates (NREL 2005)

- Capital Recovery Charge
- Raw Materials
- Process Electricity
- Grid Electricity
- Total Plant Electricity
- Fixed Costs

